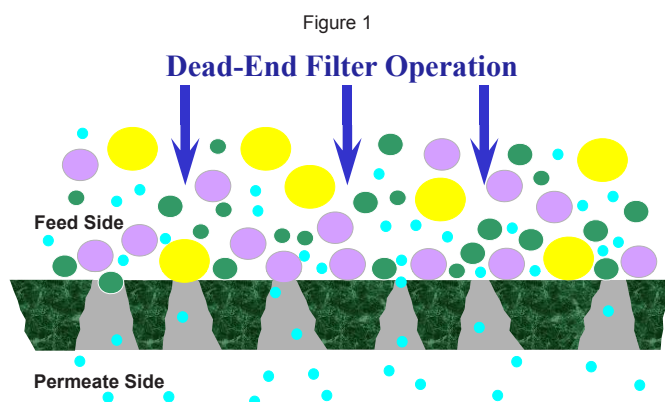


Application Bulletin

An Overview of Membrane Technology and Theory

Why Crossflow Filtration is Used

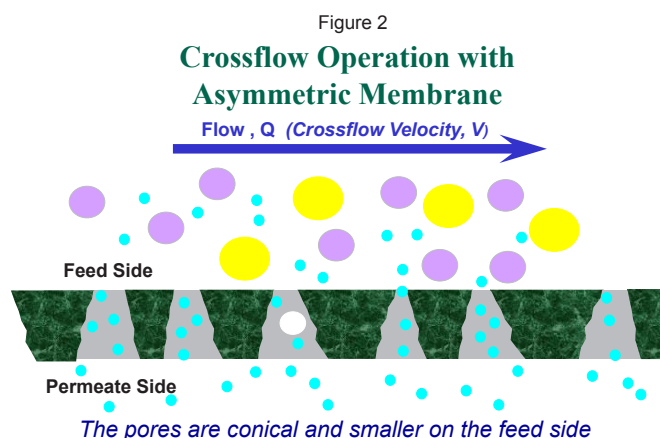
Many simple filtration processes use a dead-end technique—the flow of liquid to be filtered is directed perpendicular to the filter surface. This is effective whenever the concentration of particles to be removed is low or the packing tendency of the filtered material does not produce a large pressure drop across the filter medium. Some common examples of dead-end filtration are home water filters, vacuum cleaners and oil filters in automobiles. Typical industrial uses include the sterile filtration of water, beer, and wine.



Results in a rapid flux decline as particles accumulate.

In contrast, there are many process streams that have high concentrations of particles or macromolecules such as cells, proteins and precipitates that will rapidly compact on the filter surface when operated in a dead-end mode. Consequently, the filtration rate drops quickly to an unacceptable level. In these instances, a crossflow membrane system provides the means to maintain stable filtration rates. The key to the design of a crossflow system is selecting a membrane geometry that suits the physical characteristics of the process fluid. Crossflow membranes can be provided in tubular, flat sheet, spiral wound, and hollow fiber configurations, each of which provides certain advantages for specific process needs.

Virtually any membrane design can be applied on water-like liquids with low concentrations of suspended solids, but viscous streams and fluids with large amounts of solids can only be handled with membranes specifically designed for this purpose. In general, the more difficult a stream is to process, the higher the cost of a membrane system and the higher the operating costs. Thus, an optimization study is an important component of any potential crossflow installation.



The Evolution of Membrane Technology

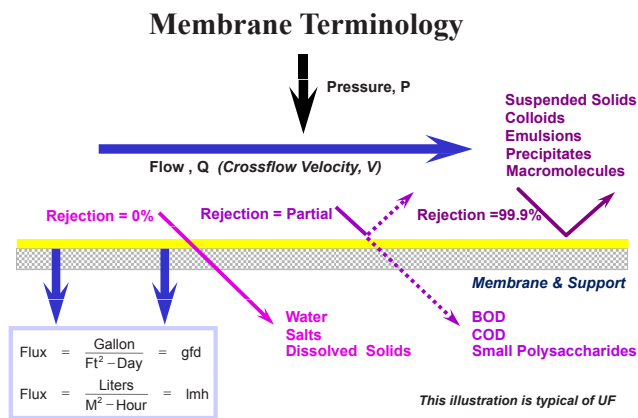
Modern crossflow technology has primarily evolved during the last forty years largely in step with the advancement of polymer chemistry. Durable, chemical-resistant polymers have made crossflow technology cost-effective. Today, 98 percent of crossflow installations utilize polymer-based membranes; inorganic materials such as ceramic are only selected in specific instances where pH, temperature, or cleaning chemistry prohibit the use of polymers.

The theoretical principles of crossflow filtration are derived from Fick's law of diffusion, which addresses the migration of suspended solids/macromolecules in a flowing stream towards a filtration surface, and the potential back-diffusion into the bulk stream. This premise forms the basis for crossflow design—that the concentration

of macromolecules at the membrane surface can be controlled as a function of the velocity of fluid flowing parallel to that surface. The design of a successful crossflow system relies on choosing a membrane geometry that can be installed and operated economically, provides consistent predictable results, and can be effectively cleaned using chemicals compatible with the membrane.

The goal of membrane technologists is to use appropriate polymer material, module configuration, system design and operating conditions to achieve the most economical process possible. At the heart of this is the selection of a membrane with the optimum separation characteristics.

Figure 3

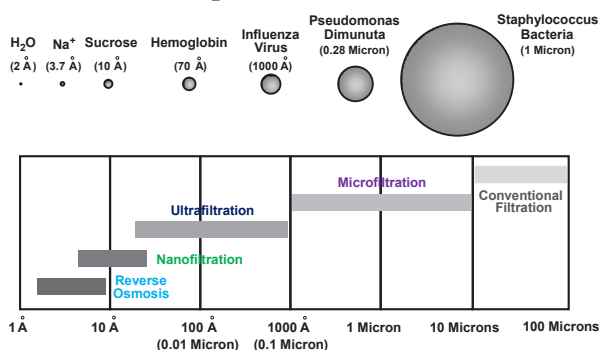


How is a Specific Membrane Process Defined?

Crossflow membranes are manufactured in a range of porosities tailored to address various applications. These span the range of salt removal from water to large particulate filtration in viscous fluids. Filtration ranges have been defined that correlate to physical aspects of the membrane process and the relative size exclusion involved. In addition to the choices of polymer and membrane geometry, pore size selection is an integral part of process optimization.

Figure 4

Comparative Dimensions

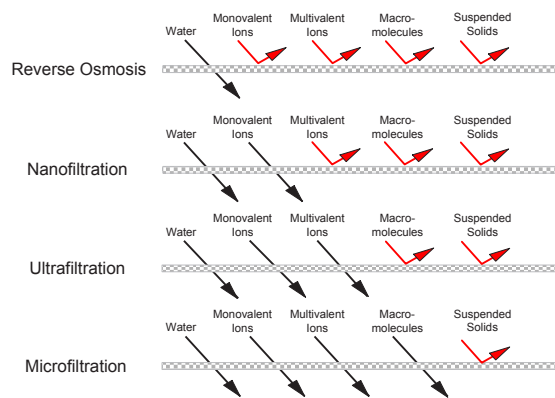


The membrane regime with the smallest pores is reverse osmosis (RO), which involves—appropriately enough—reversal of the osmotic pressure of a solution in order to drive water away from dissolved molecules. Strictly speaking, RO is not a size exclusion process based on pore size; it depends on ionic diffusion to effect the separation. A common application of reverse osmosis is seawater desalination in which pure water is produced from a highly saline feed stream. In applications such as this, reverse osmosis serves a similar purpose to evaporation, yet provides better economics.

RO is also used in many industrial processes including cheese whey concentration, fruit juice concentration, ice-making, and car wash reclamation, and wastewater volume reduction. In each of these examples, the goal is either to produce a pure filtrate (typically water) or retain entirely the components of the feed stream as the product. Because the osmotic pressure (a measure of the dissolved ion concentration) of many process streams is quite high, RO membranes must be designed to operate at pressures of 400-1200 psi (29-83 bars) which restricts the available membrane geometries.

Figure 5

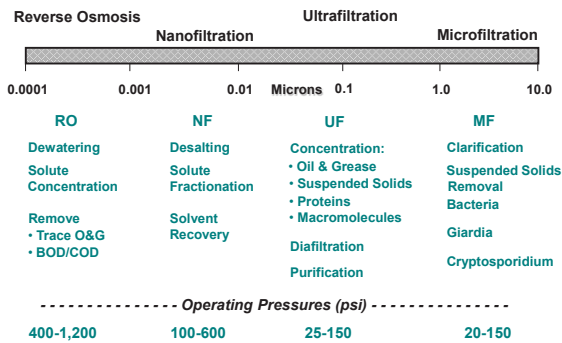
Relative Size Exclusion



A natural extension of reverse osmosis is nanofiltration (NF)—the most recent development on the crossflow frontier. NF functions similarly to reverse osmosis, but is generally targeted to remove only divalent and larger ions, hence the nickname for NF—selective reverse osmosis. Monovalent ions such as sodium and chloride will pass through a nanofiltration membrane, thus many of the uses of NF involve de-salting of the process stream. An example is the production of lactose from cheese whey; the NF process is designed to concentrate the lactose molecules while passing salts—a procedure that purifies—and concentrates—

the lactose stream. In water treatment, NF membranes are used for hardness removal (in place of water softeners), pesticide elimination and color reduction. Nanofiltration can also be used to reclaim spent NaOH solutions. In this case, the permeate (filtrate) stream is purified NaOH, allowing reuse many times over.

Figure 6
Crossflow Applications



NF is also an osmotic pressure-dependent process, but due to the passage of monovalent ions, the net osmotic driving force required is less than RO. Operating pressures are lower and filtration rates are higher. Nanofiltration membranes typically operate in the range of 100-600 psi (7-42 bars). In many instances, NF can be used in place of RO.

Following the progression in the Relative Size Exclusion chart, ultrafiltration (UF) is the next process on the pore size continuum. UF is not an osmotic process—the pores of UF membranes are larger and the method of rejection is primarily physical size exclusion. While RO/NF membranes are generally categorized by the degree of salt rejection under standard conditions, UF membranes are specified by a molecular weight cut-off rating (MWCO). The range of MWCOs for UF is generally considered to be 1,000-1,000,000 Daltons which can be loosely correlated to pore size (roughly equivalent to 0.005-0.1 microns).

The major opportunities for UF involve clarification of solutions containing suspended solids, bacteria or high concentrations of macromolecules. These include oil/water separation, fruit juice clarification, milk and whey production, automotive electrocoat paint filtration, purification of pharmaceuticals, poly-vinyl alcohol and indigo recovery, potable water production, and tertiary wastewater reuse.

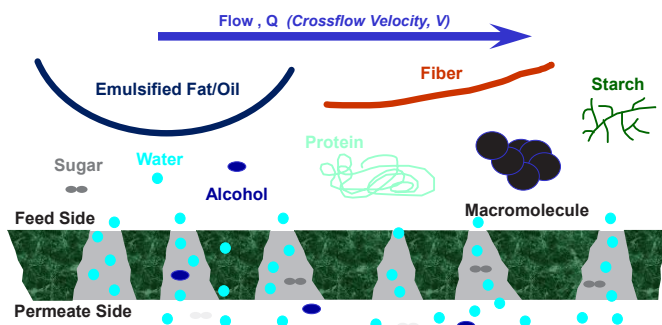
UF membranes are manufactured in a much larger variety of configurations to address the wide range of applications. Many membrane geometries are available in part due to the fact that UF processes operate below 150 psi (10 bars)—some as low as 25 psi (2 bars).

The last sector that pertains to crossflow technology is microfiltration (MF). MF is actually a hybrid, having its significant applications in simple dead-end filtration for water filtration, sterile bottling of fruit juices and wine, and aseptic uses in the pharmaceutical industry. However, not all applications that benefit from the use of MF operate successfully in the dead-end mode; a large portion of the MF market has been captured by crossflow.

The most common of these are clarification of whole cell broths and purification processes in which macromolecules must be separated from other large molecules, proteins and/or cell debris. Clarification of dextrose and highly-colored fruit juices employ MF extensively as well. There are also large markets for MF crossflow filtration in wine production, milk/whey de-fatting, and brewing.

As with UF, MF systems operate at relatively low pressures and there are a variety of membrane configurations commercially available.

Figure 7
UF Membrane Example Size Exclusion



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